

Indus Engineering

Heat Exchanger Design Case Study

Condenser for Medical Device Cooling System

Customer Requirement

- ❑ Development of condenser coil of medical device cooling system
- ❑ Use of next generation low GWP refrigerant gas to reduce environmental impact of HFC
- ❑ Reduction of material cost and refrigerant charge



Task

- **Design of condenser coil with low GWP refrigerant R290**

 - **Task is to achieve:**
 - **Maximum performance keeping low refrigerant charge within safety limit**
 - **Minimum pressure drop both air side and refrigerant side**
 - **Lower superheating and subcooling values**
 - **Mounting of condenser within existing coil envelope**
-

Actions

❑ Indus Engineering team took up the challenge and with our software simulation program and HVAC/ refrigeration system knowledge, condenser design were carried out

❑ Tube diameter selection:

- Simulation with different tube diameter to minimize internal volume of coil
- Minimisation of refrigerant charge of R290 refrigerant
- Keeping desired performance of coil at different ambient conditions

CONDENSING COIL - 20 x 17.32 x 5mm IG x LF 13T 2NR 336A 1.5P 1NC			
Geometry	17.32 x 5mm IG x LF	Coil Length	336.0 mm
Nr of Tubes per Row	13	Fin Pitch	1.50 mm
Nr of Rows	2	Nr of Circuits	1
Capacity		Tube Shape	Circular
Exchange Surface	42.446		Btu/h
Global Exchange Coefficient	8.76		ft ²
DTML	3.1		Btu/(h ft ² °F)
Fins Material / Tubes Material	Aluminium / Copper		K
Fin Thickness	0.00472		in
Coil Internal Volume	0.005		ft ³
Tubes External Diameter	0.1969		in
Tubes Internal Diameter	0.1748		in
Number of skipped tube	0		
AIR SIDE			
Atmospheric Pressure / Altitude	14.70 / 0.00		psi / ft
Volumetric Air Flow	390.0		cfm/min
Mass Air Flow	1674.78		lb/h
Face Velocity on the Coil	2.11		m/s
Inlet Air Density	0.071572		lb/ft ³
Inlet Air Temperature	32.0		°C
Inlet Air Relative Humidity	50.00		%
Inlet Air Specific Humidity	103.30		gr/lb AS
Inlet Air Enthalpy	37.73917		Btu / lb
Outlet Air Temperature	34.8		°C
Outlet Air Relative Humidity	42.79		%
Outlet Air Specific Humidity	103.30		gr/lb AS
Outlet Air Enthalpy	38.97263		Btu / lb
Pressure Drop	28		Pa
Partial Exchange Coefficient	12.25		Btu/(h ft ² °F)
Fouling Factor	0.0000		(ft ² h °F)/Btu
REFRIGERANT SIDE			
Fluid		PROPANE	
Mass Fluid Flow	11.93		lb/h
Fluid Velocity (Gaseous Phase)	3.47		m/s
Fluid Velocity (Liquid Phase)	0.21		m/s
Mass velocity	97		kg/(m ² s)
SubCooling	1.5		K
Desuperheating	40.0		K
Condensing Temperature	37.0		°C
Fluid Pressure Drop	22.34		kPa
Manifold Pressure Drop	0		kPa
Total Pressure Drop Fluid Side	22.34		kPa
Partial Exchange Coefficient	594.86		Btu/(h ft ² °F)
Fouling Factor	0.0000		(ft ² h °F)/Btu

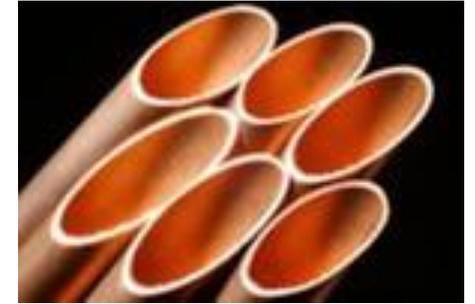
Actions

□ **Fin Selection:**

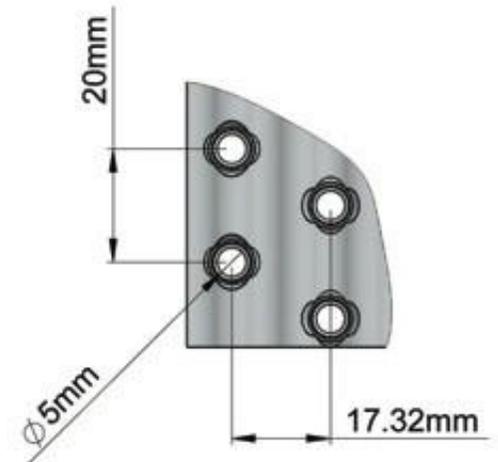
- **Performance simulation carried out with different fin geometry**
- **Keeping wide fin spacing**
- **Meet low air side pressure drop**

Solution

- Based on various iterations, we choose two geometries:
 1. Mini-channel tube of 5mm OD and compact fin geometry pattern 20 x 17.32mm and sine wave type fin
 2. Tube of 7mm OD and fin geometry pattern 25 x 21.65mm and sine wave type fin



5MM DIA TUBES



Solution

- ❑ **Compressor flow rate design:**
 - Refrigerant flow rate is designed for a certain level of superheating and subcooling
- ❑ **A complete matrix of simulation results was prepared with various options**
- ❑ **After deliberation, optimum performance and cost viable option is selected with 5mm OD tube**

Solution

- ❑ **Coil circuit designed to keep refrigerant side pressure drop optimum**
- ❑ **Sampling and testing were carried out at customer end and coils performed as per desired target**

Benefits

- ❑ **Achieved targeted performance of condenser keeping refrigerant charge within safety limit**
- ❑ **Cost Effective Solution:**
 - **Reduction in material weight by 12% and cost reduction by 15%**
 - **Low refrigerant charge**
- ❑ **Meeting EU f-gas regulations of low GWP refrigerant using R290 compared to R410a**